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CONJUGATE HEAT TRANSFER ANALYSIS
OF THERMAL MANAGEMENT OF
A LI-ION BATTERY PACK

by

DIVYA CHALISE

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The University of Texas at Arlington in Partial Fulfillment
of the Requirements
for the Degree of

HONORS BACHELOR OF SCIENCE IN MECHANICAL ENGINEERING

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November 25, 2017

ABSTRACT

CONJUGATE HEAT TRANSFER ANALYSIS OF THERMAL MANAGEMENT OF A LI-ION BATTERY PACK

Divya Chalise, B.S. Mechanical Engineering

The University of Texas at Arlington, 2018

Faculty Mentor: Ankur Jain

Thermal management of Li-ion battery packs is a critical technological challenge that directly impacts safety and performance. Removal of heat generated in individual Li-ion cells into the ambient is a considerably complicated problem involving multiple heat transfer modes. This work develops an iterative analytical technique to model conjugate heat transfer in coolant-based thermal management of a Li-ion battery pack. Solutions for the governing energy conservation equations for thermal conduction and convection are derived and coupled with each other in an iterative fashion to determine the final temperature distribution. The analytical model is used to investigate the dependence of the temperature field on various geometrical and material parameters. This work shows that the coolant flowrate required for effective cooling can be reduced significantly by improving the thermal conductivity of individual Li-ion cells. Further, this work helps in

understanding key thermal-electrochemical trade-offs in the design of thermal management for Li-ion battery packs, such as the trade-off between temperature rise and energy storage density in the battery pack.

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CHAPTER 1

INTRODUCTION

Effective removal of heat from Li-ion cells and battery packs is a critical technological challenge for improving the performance, safety and reliability of electrochemical energy conversion and storage systems [1-3]. Several engineering applications such as electric vehicles and stationary power storage systems involve large battery packs containing multiple Li-ion cells capable of individually storing and converting energy. Heat generated within each Li-ion cell during charge/discharge must be eventually rejected to the ambient. This process must occur with minimal thermal resistance in order to minimize the temperature rise in each Li-ion cell [4,5]. The path of heat transfer from within each cell to the ambient is somewhat involved [6]. During this process, heat must conduct through materials and interfaces within each cell, then into any surrounding materials, followed by convection into the coolant fluid, which carries the heat away from the battery pack and eventually rejects it to the ambient [7]. Pack-level thermal management plays a key role in overall thermal performance of a battery pack [3]. However, effective, active thermal management may require components such as coolant channels and pump that do not contribute to energy storage and may even consume energy. While the thermal management system must ensure effective heat removal, the non-electrochemical components in the pack must be minimized in order to increase the energy storage density and reduce overall weight. The development of accurate thermal modeling tools is critical for reconciling such design trade-offs and designing battery packs that can

maximize energy storage density while limiting the temperature rise and temperature gradient within the pack.

Significant past work is available on both experimental measurements and modeling of pack-level thermal management of Li-ion battery packs. A variety of thermal management approaches, including heat pipe-based cooling and convective cooling, has been investigated. Both air and liquid-based thermal management has been demonstrated experimentally for Li-ion battery packs [8-14]. Water is the most commonly investigated liquid coolant. The use of liquid cooling plates has also been investigated. Various cell arrangements in a Li-ion battery pack along with different cooling duct configurations have been experimentally evaluated for air cooling [8-11]. Similarly, liquid-based cooling using cooling plates with microchannels of different configurations placed between batteries has been reported [12-14]. Some work also exists on the use of low boiling-point dielectric liquids for thermal management [15-16]. Heat pipes and phase change materials have been inserted in the battery pack in order to absorb heat generated in the cell and minimize temperature rise [17-30]. A number of papers have utilized finite-element simulations to numerically characterize the performance of such thermal management systems. Air [10-11,21-36], liquid [12-14, 37-40], heat pipe [36] and Phase Change Materials [27,41,42] based thermal management approaches have been evaluated by pack-level simulations. The modeling of different cooling configurations [31-33], cell arrangements [10-11,34] and flow duct design [32] for enhanced natural convection has been carried out. Similarly, liquid cooling based thermal management strategies have been analyzed through simulations. These include design of liquid cooling plate [12,13,38-40], thermal optimization [38-40] and evaluation of different cooling strategies [14,37]. Numerical

simulations on the use of Phase Change Materials [41,42] and heat pipes [36] for pack-level thermal management have also been reported. While these simulation-based studies show significant reduction in temperature of the battery pack, they often neglect the impact of these cooling strategies on reduction in pack level energy storage density.

While finite-element simulations offer convenience in determining the temperature rise in a specific geometry, such simulations can often be time-consuming to set up and execute. More importantly, there are often challenges in interfacing such simulations with the battery management system (BMS), which is a critical need for thermally-driven battery performance management. An alternative to finite-element simulations is analytical derivation of the solution of energy conservation equations that govern the temperature field in the system. While mathematically more challenging, such an analytical modeling approach results in closed-form solutions of the temperature distribution that provide useful physical insights into the heat transfer process that is not possible through simulations. For example, once a closed-form solution for the temperature field is available, the effect of various geometrical parameters and thermophysical properties can be rapidly evaluated. Closed-form solutions are also easier to interface with other computational tools, such as electrochemistry models, for multiphysics co-optimization during the design process, or during real-time operation. However, analytical approaches are mathematically more challenging than finite-element simulations, and geometrical approximations may be needed. Air/liquid cooling of a Li-ion battery pack is a conjugate heat transfer problem involving both thermal conduction in the solid battery and thermal convection to the coolant flow. The modeling of such conjugate problems is not straightforward. While conjugate heat transfer models have been developed for simple conditions, there is

relatively limited work available on analyzing conjugate heat transfer in more complicated situations such as those that may be encountered in realistic battery packs. In the recent past, a general, iterative method has been developed for analytical modeling of conjugate heat transfer in solid-fluid domains [43] such as the cooling of Li-ion cells using a coolant flow. This method is based on solving the thermal conduction and convection problems separately. Utilizing temperature and heat flux matching at the solid-liquid interface, the output of one problem is utilized to solve the other in an iterative fashion. This approach has been shown to work well for a broad class of conjugate problems involving external and internal flow [43].

This work presents conjugate heat transfer analysis for the cooling of a Li-ion cell battery pack. An iterative analytical approach, validated in a variety of ways, is used to investigate fundamental processes that govern temperature rise in a Li-ion battery pack. The dependence of the temperature field on various geometrical and material parameters is investigated. The analytical model helps understand thermal management of Li-ion battery packs, and assists in understanding and quantifying various thermal-electrochemical tradeoffs that arise in the design of a Li-ion battery pack. These results may contribute towards improved thermal design and run-time thermal performance of Li-ion battery packs.

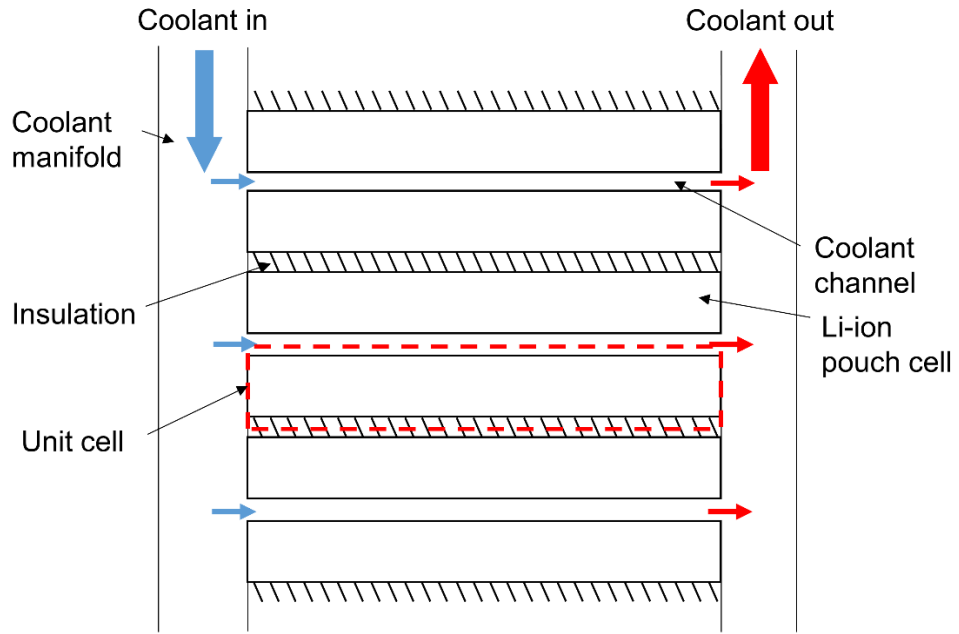


Figure 1.1: Battery Pack Geometry and Unit Cell

CHAPTER 2

THEORETICAL MODEL

The problem of cooling of a Li-ion cell in a battery pack with a fluid flow such as air or water is shown schematically in Figure 1.1, where multiple cells in a battery pack are to be cooled. Figure 1.1 also identifies the unit cell that repeats itself in the battery pack. The temperature field within this unit cell is to be determined as a function of geometry, operating parameters of the cell, such as C-rate, thermal properties, as well as the parameters and properties related to the coolant fluid. This is a conjugate heat transfer problem as it involves heat transfer through conduction within the solid cell and convective heat transfer to the cooling fluid. While problems involving conduction or convection only are easier to address by directly solving the underlying energy conservation equation in the solid or liquid, a conjugate problem is considerably more complicated due to the interaction between the solid and fluid. In this case, an iterative analytical technique is utilized for solving the conjugate problem [43].

The technique utilizes continuity of temperature and energy conservation at the solid-liquid interface to iteratively solve the conduction and convection problems separately [43]. The solution of each problem provides a boundary condition for the other problem. The iterative solution process continues until sufficient accuracy is reached.

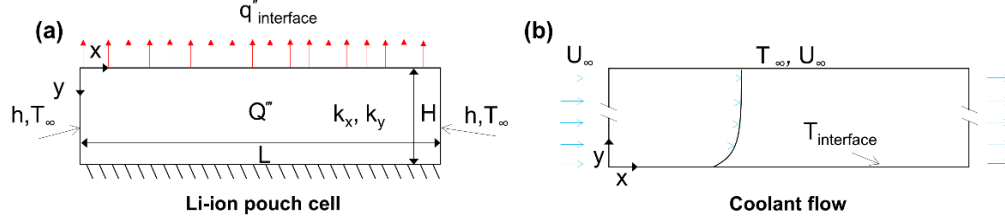


Figure 2.1: Definitions of the Individual (a) Solid and (b) Fluid Problems

In this specific case, Figure 2.1 (a) shows the solid domain of the conjugate problem in the thermal unit cell. The steady state temperature rise in the solid domain, $T_s(x,y)$, satisfies the following energy conservation equation:

$$k_{x,s} \frac{\partial^2 T_s}{\partial x^2} + k_{y,s} \frac{\partial^2 T_s}{\partial y^2} + Q''' = 0 \quad (1)$$

In addition, the following boundary conditions are also satisfied:

$$k_{x,s} \frac{\partial T_s}{\partial x} = hT_s \quad \text{at } x = 0 \quad (2)$$

$$-k_{x,s} \frac{\partial T_s}{\partial x} = hT_s \quad \text{at } x = L \quad (3)$$

$$\frac{\partial T_s}{\partial y} = 0 \quad \text{at } y = 0 \quad (4)$$

$$-k_{y,s} \frac{\partial T_s}{\partial y} = q_0''(x) \quad \text{at } y = H. \quad (5)$$

$q_0''(x)$ is the heat flux at the solid-fluid interface, and it is not known in advance. The fluid domain of the thermal unit cell comprises the coolant flow shown in Figure 2.1 (b).

The temperature field in the fluid domain is governed by

$$\alpha_f \frac{\partial^2 T_f}{\partial y^2} = u \frac{\partial T_f}{\partial x} + v \frac{\partial T_f}{\partial y} \quad (6)$$

where viscous dissipation is neglected.

Finally, at the solid-fluid interface, temperature continuity and conservation of energy respectively give

$$T_f = T_s \quad (7)$$

and

$$k_{y,s} \frac{\partial T_s}{\partial y} = k_f \frac{\partial T_f}{\partial y}. \quad (8)$$

The conjugate problem described in equations (1)-(8) is solved in an iterative approach. For the fluid domain, equation (6) is solved for a flow over a flat plate problem with an assumed temperature distribution $T_0(x)$ so that

$$T_f = T_0(x). \quad (9)$$

A solution for this problem has been derived by integrating the effect of infinitesimal sections of the flat plate with given temperature rise of the interface [44]. The final solution for the temperature distribution in the coolant fluid is given by [44]

$$T_f(x, y) - T_e = \int_0^x [1 - \theta(\xi, x, y)] \frac{dT_{wall}}{d\xi} d\xi + \sum_{i=1}^k [1 - \theta(\xi_i, x, y)] (T_{wall}(i) - T_e) \quad (10)$$

where the function $\theta(\xi, x, y)$ is given by

$$\theta(\xi, x, y) = \frac{T_{wall} - T_f}{T_{wall} - T_e} = \frac{0.331 \text{Pr}^{1/3} \text{Re}_x^{1/2} y}{x \left[1 - \left(\frac{\xi}{x} \right)^{3/4} \right]^{1/3}} - \frac{0.005405 \text{Pr} \text{Re}_x^{3/2} y^3}{x^3 \left[1 - \left(\frac{\xi}{x} \right)^{3/4} \right]} \quad (11)$$

In equation (10), the integration and the summation accounts for the continuous variation and step changes in T0 respectively. This equation assumes that the dimensions of the coolant channel cross-section are larger than the expected maximum boundary layer size. The interface heat flux can be computed from equations (10) and (11) as follows [44]:

$$q_{wall}(x) = -k_y \left. \frac{\partial T_f}{\partial y} \right|_{y=0} = k_y \left[\int_0^x \frac{\partial \theta}{\partial y}(\xi, x, 0) \frac{dT_{wall}}{d\xi} d\xi + \sum_{i=1}^k \frac{\partial \theta}{\partial y}(\xi_i, x, 0)(T_{wall}(i) - T_e) \right] \quad (12)$$

This heat flux is used to solve the solid problem defined by Equations (1)-(5) by first splitting the problem into two problems followed by the use of separation of variables technique [45]. The temperature rise in the solid domain, Ts(x,y) can be determined by splitting into two components [45]:

$$T_s(x, y) = s(x) + w(x, y). \quad (13)$$

The two components of the temperature distribution are given by

$$s(x) = \frac{Q'''}{2k_{x,s}} \left[x(L-x) + \frac{L^2}{Bi_L} \right] \quad (14)$$

and

$$w(x, y) = \sum_{n=1}^{\infty} C_n \text{Cosh} \left(\sqrt{\frac{k_{x,s}}{k_{y,s}}} \mu_n y \right) \cdot [\mu_n L \text{Cos}(\mu_n x) + Bi_L \text{Sin}(\mu_n x)]. \quad (15)$$

The coefficients Cn in equation (15) are given by

$$C_n = \frac{-\frac{1}{L} \int_0^L q(x) \cdot [\mu_n L \text{Cos}(\mu_n x) + Bi_L \text{Sin}(\mu_n x)] dx}{\frac{1}{2} \cdot \left[(\mu_n L)^2 + Bi_L^2 \right] \left(1 + \frac{Bi_L}{(\mu_n L)^2 + Bi_L^2} \right) + Bi_L} \cdot \left[\mu_n \sqrt{\frac{k_{x,s}}{k_{y,s}}} k_y \text{Sinh} \left(\sqrt{\frac{k_{x,s}}{k_{y,s}}} \mu_n H \right) \right] \quad (16)$$

The eigenvalues μ_n are obtained from roots of the transcendental equation

$$\tan(\mu L) = \frac{2Bi_L \cdot (\mu L)}{(\mu L)^2 - Bi_L^2}, \quad (17)$$

where

$$Bi_L = \frac{hL}{k_{x,s}}. \quad (16)$$

In the solid problem, the interface temperature distribution $T_0(x)$ is calculated by substituting $y=H$ in equation (13), which is provided to equation (9) as $T_0(x)$ to re-solve the fluid problem. The iterative process is continued until convergence is reached. In practice, the interface temperature distribution is updated to a blend of the newly calculated and older distributions. If $T_{0,old}(x)$ represents the interface temperature at the present iteration, the new interface temperature distribution is obtained by

$$T_{0,new}(x) = \alpha T_s(x, y = H) + (1 - \alpha) T_{0,old}(x). \quad (16)$$

The blend factor α is kept low enough in order to prevent divergence in the temperature distribution with increasing number of iterations.

In summary, the iterative approach utilized here starts with an assumed temperature profile at the solid-fluid interface, solves the fluid problem to provide a heat flux input that enables the solution of the solid problem [43]. The solution for the solid problem is then used to determine a new temperature profile at the solid-fluid interface. This process is repeated iteratively until convergence [43]. Figure 2.2 shows a schematic of this iterative procedure.

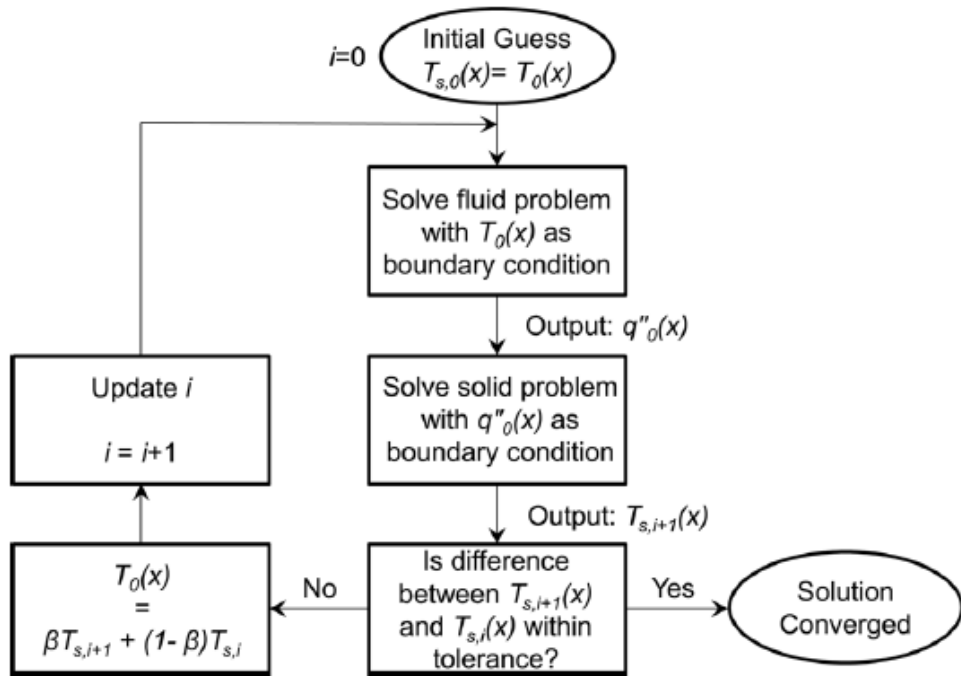


Figure 2.2: Schematic of the Iterative Procedure

CHAPTER 3

RESULTS AND DISCUSSION

The analytical model described in Section 2 is validated in a number of different ways. A conjugate heat transfer problem with parameters representative of water cooling of prismatic Li-ion cells discharging at 5C is solved. Based on recently presented data on heat generation rate measurement [46], this C-rate corresponds to a heat generation rate of 98.5 kW/m^3 . Thermal properties of the Li-ion cell are taken from recent measurements [47]. Specifically, thermal anisotropy is assumed, with the thermal conductivity parallel and normal to the electrode plane assumed to be 30.0 and 0.2 W/mK respectively. The cell thickness is taken to be 8mm. The coolant flow speed is assumed to be 0.001 m/s. The ambient temperature is assumed to be 25 °C in all cases considered in this section, so that standard room temperature values for various thermophysical properties of the coolant air are used.

The iterative analytical approach is carried out three separate times assuming three different initial values for the interface temperature. Figure 3.1 plots the interface temperature as a function of x for all three cases at the end of a number of iterations. Figure 3.1 shows that for each case, the temperature distribution converges within around 30 iterations and does not change significantly afterwards. Based on this, the number of iterations is conservatively taken to be 60 for subsequent investigations in this work. Figure 3.1 also shows that the temperature distribution converges to the same curve regardless of

the initially assumed temperature distribution. This independence from the initial guess is important and ensures a robust solution even if the initial guess is far from the actual temperature distribution.

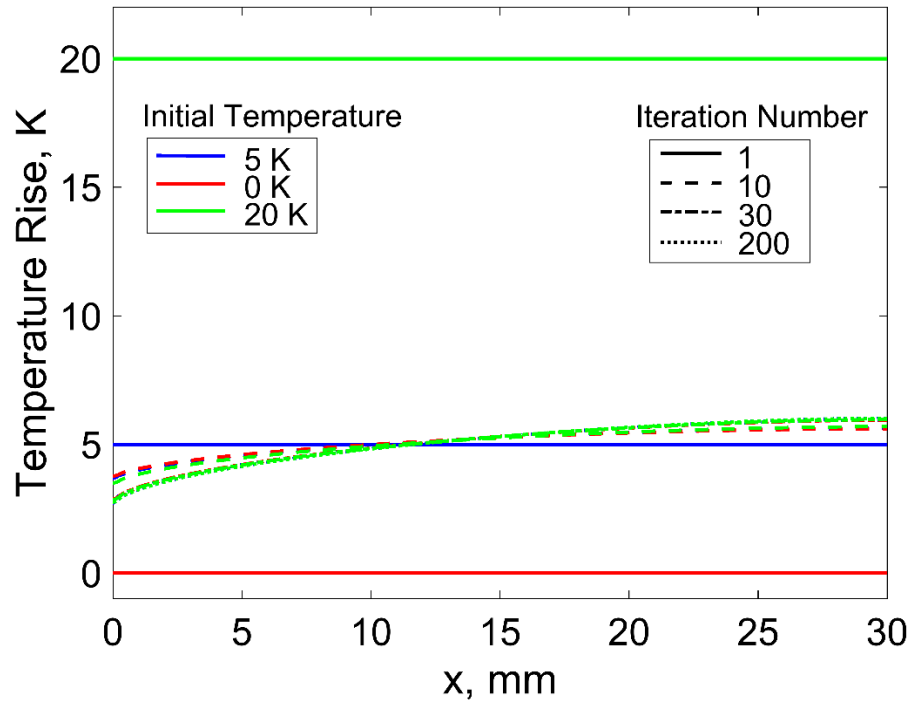


Figure 3.1: Temperature Convergence with Three Different Initial Temperatures

While the solution for the thermal conduction equation in the solid body comprises a series summation of infinite terms, this series must in practice be truncated to a finite number of terms. Figure 3.2 plots the converged temperature distribution at the interface for the problem with the same parameters as Figure 3.1 for different numbers of eigenvalues. Figure 3.2 shows that the temperature solution changes rapidly at low number of eigenvalues, but converges to a stable solution at around 50 eigenvalues. Addition of further eigenvalues does not significantly change the predicted temperature distribution. This is an important observation for reducing computational burden without significant

penalty in accuracy. Based on this, a total of 50 eigenvalues are considered in all subsequent figures in this thesis.

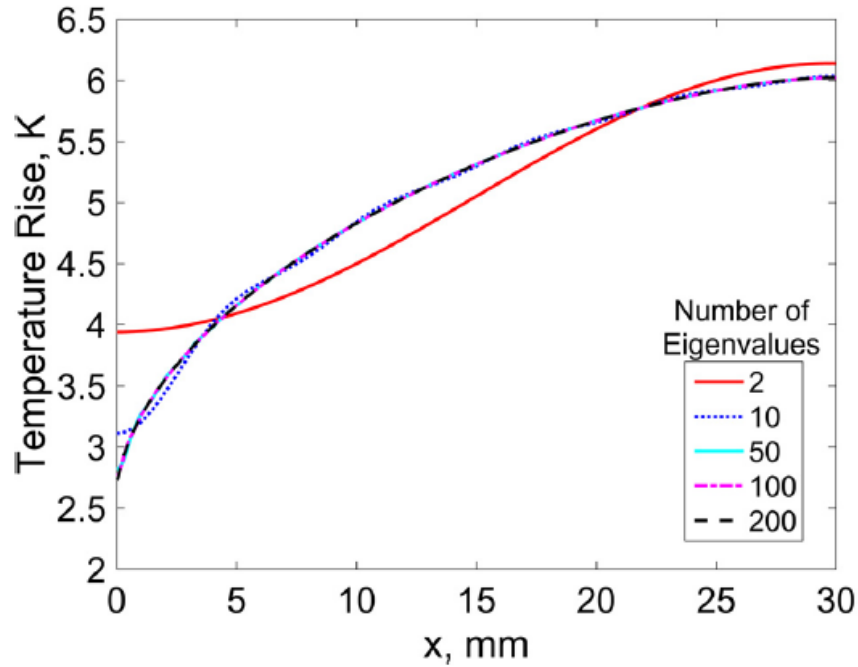


Figure 3.2: Temperature Convergence with Increase in Number of Eigenvalues

The iterative technique for determining temperature distribution during Li-ion cell cooling is also validated by comparison with finite-element simulations. These simulations utilize the same set of parameters as in the iterative technique. A total of around 500 K elements are used and grid independence is verified. Meshing is refined sufficiently to capture high heat transfer rate near the leading edge, and to capture boundary layer effects in the fluid domain close to the solid-fluid interface. The fluid domain is defined to be much larger than expected thickness of velocity and thermal boundary layers. Figure 3.3(a) plots the interface temperature as a function of x for two different C-rates, 4C and 5C, utilizing the same 0.001 m/s water flow for cooling. The heat generation rates at 4C and 5C are 67.8 kW/m³ and 98.5 kW/m³ respectively [46]. Plots from both finite-element

simulations and the analytical model are shown. Figure 3.3(a) shows very good agreement between the two. Further, the heat flux from the solid into the coolant fluid is also plotted as a function of x for finite-element simulations and analytical model in Figure 3.3(b). Similar to the temperature distribution, there is very good agreement for the heat flux distribution. Compared to finite-element simulations, the iterative analytical model offers improved computation time, elimination of the need for time-consuming grid generation and a better physical insight into the conjugate problem that governs fluid cooling of a Li-ion cell.

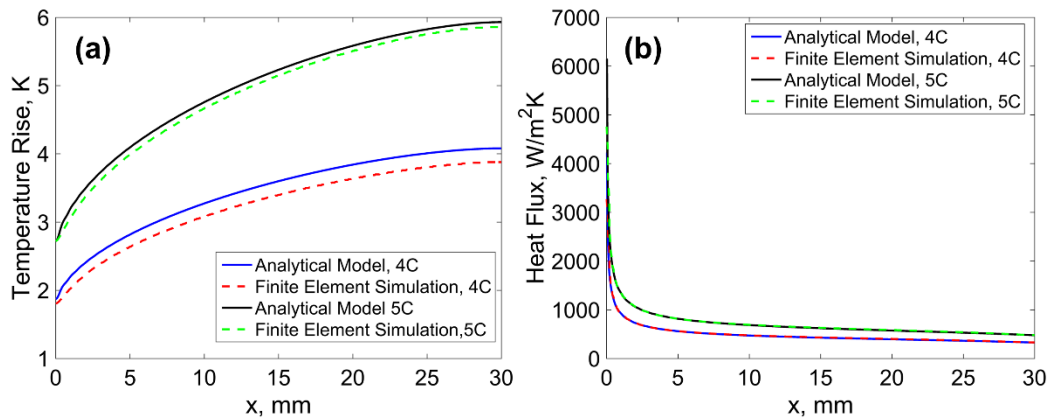


Figure 3.3: (a) Temperature and (b) Heat Flux Agreement with FEM Model

The validated analytical model can be utilized for pack-level thermal design. Specifically, the dependence of thermal performance on various parameters such as geometry and thermophysical properties can be effectively analyzed. Figure 3.4(a) plots a colormap of the entire cell for a specific case of 5C operation corresponding to 98.5 kW/m^3 while being cooled with 0.001 m/s water flow. The temperature plot in Figure 3.4(a) clearly shows temperature rise within the cell due to heat generation, and the cooling effect of the coolant flow. Figure 3.4(b) further illustrates the temperature field by plotting the

temperature rise as a function of y at $x=15$ mm. Starting from the surface of the cell, the temperature rise increases going inwards, and is the highest at the core of the cell, as expected.

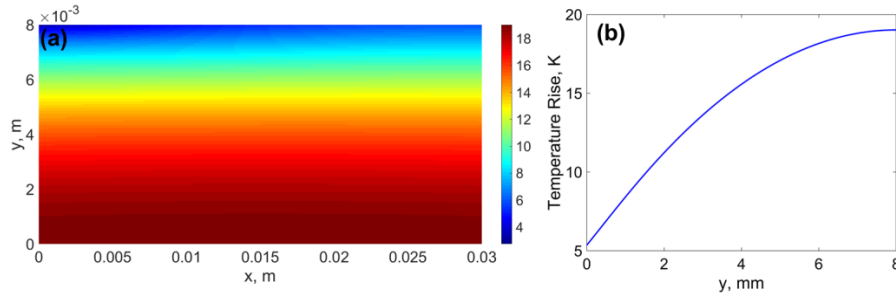


Figure 3.4: Temperature Distribution (a) Within the Cell and (b) Along y -axis

A number of other investigations of pack-level thermal management are possible through the iterative analytical model. Figure 3.5(a) plots the peak temperature inside the prismatic cell as a function of C-rate for two different flowrates of water as a coolant. This plot shows a sharp increase in peak temperature rise at the core of the cell with increasing C-rate, which is along expected lines, since the heat generation rate increases quadratically with C-rate [46]. Figure 3.5(b) plots the peak temperature as a function of flowrate for water as the coolant over a prismatic cell operating at two different C-rates. This plot shows a reduction in peak temperature as the coolant flow increases, but this effect saturates somewhat at higher flowrates. This shows that merely increasing the coolant flowrate does not necessarily keep improving the overall performance but rather results in diminishing returns at large flowrates. The temperature rise does not drop to insignificant levels at higher flowrates because the non-zero thermal resistance within the cell material remains constant regardless of the coolant flowrate outside the cell.

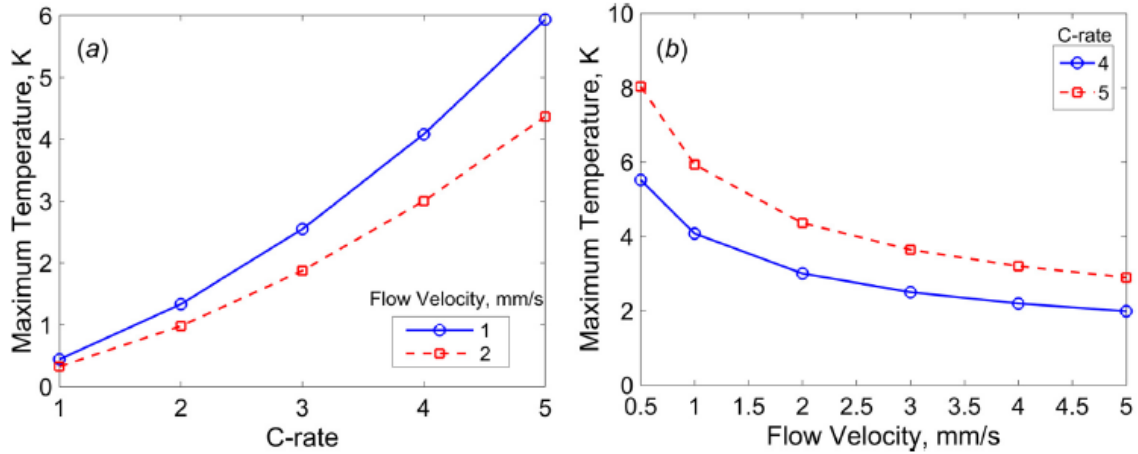


Figure 3.5: Maximum Temperature Rise with Varying (a) C-rate and (b) Flow Velocity

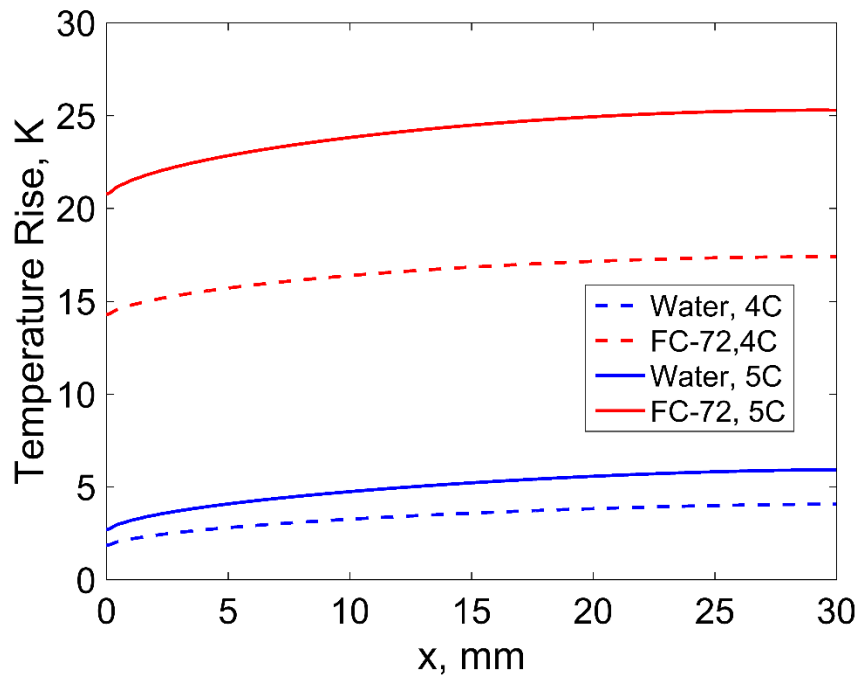


Figure 3.6: Interface Temperature as Function of x for Water and FC-72

It is of interest to compare the performance of various coolant fluids. Figure 3.6 plots the surface temperature as a function of x for two different C-rates, and compares the performance of water and FC72, a dielectric fluid. Figure 3.6 shows that for both C-rates, the temperature rise is lower for water compared to FC72, due to superior thermophysical

properties of water. A key drawback with water, however, is the potential for electrical damage in case of leakage. Due to its inherently dielectric nature, FC72 does not present this risk, but has somewhat lower thermal performance.

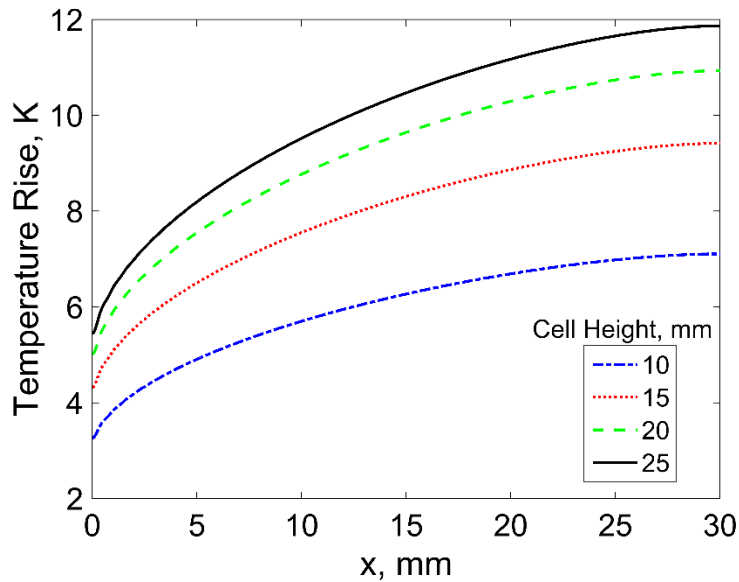


Figure 3.7: Temperature Rise with Varying Cell Height

The iterative analytical model can also be used to study the effect of geometry on the thermal performance of the coolant flow. Figure 3.7 plots the surface temperature of the Li-ion cell as a function of different widths of the Li-ion cell, holding the volumetric heat generation rate constant at 98.5 kW/m^3 . Figure 3.7 shows that, at the same C-rate, a thicker cell results in greater temperature rise than a thinner cell. This means a thicker cell will also result in higher pack-level energy storage density, which, while desirable, comes at the cost of increased peak temperature in thicker cells.

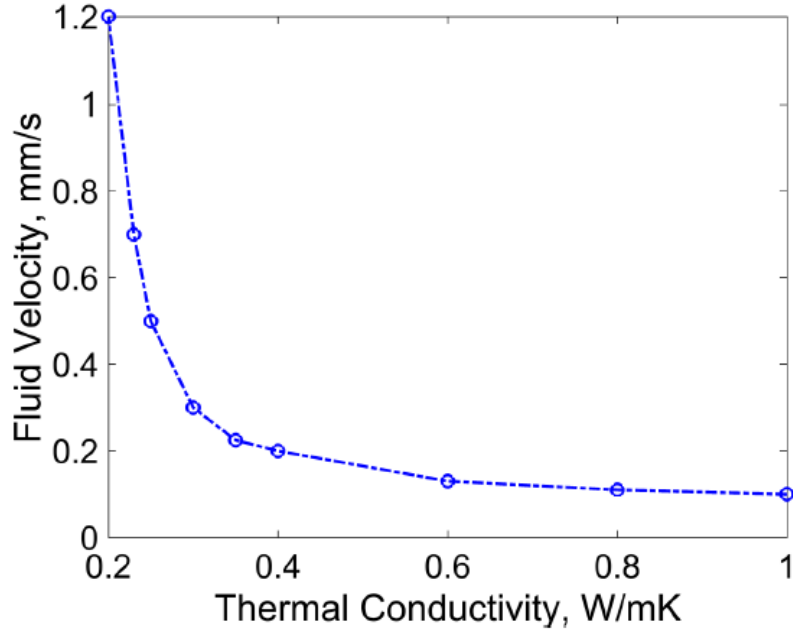


Figure 3.8: Fluid Velocity for a Certain Temperature Rise with Varying k_y

Strategies for the enhancement of the thermal conductivity of Li-ion cells have been proposed in the past [6]. It is of interest to analyze the impact of such cell-level enhancement on pack-level thermal management. An analysis is carried out to determine the required coolant fluid velocity for multiple values of the cell thermal conductivity $k_{y,s}$ in order to maintain the same maximum temperature rise in the cell as a baseline case. A heat generation rate of 98.5 kW/m³ corresponding to discharge rate of 5C is used here. Results presented in Figure 3.8 show a significant reduction in the required fluid velocity as $k_{y,s}$ increases from 0.2 W/mK to 0.4 W/mK. However, further increase in thermal conductivity is not found to be as advantageous, because convective heat transfer resistance now begins to dominate over thermal conduction resistance. This analysis shows that increased thermal conductivity of constituting Li-ion cells may positively impact system

level coolant flow requirements such as pump work, size of coolant manifold, etc. and ultimately the pack-level energy storage density.

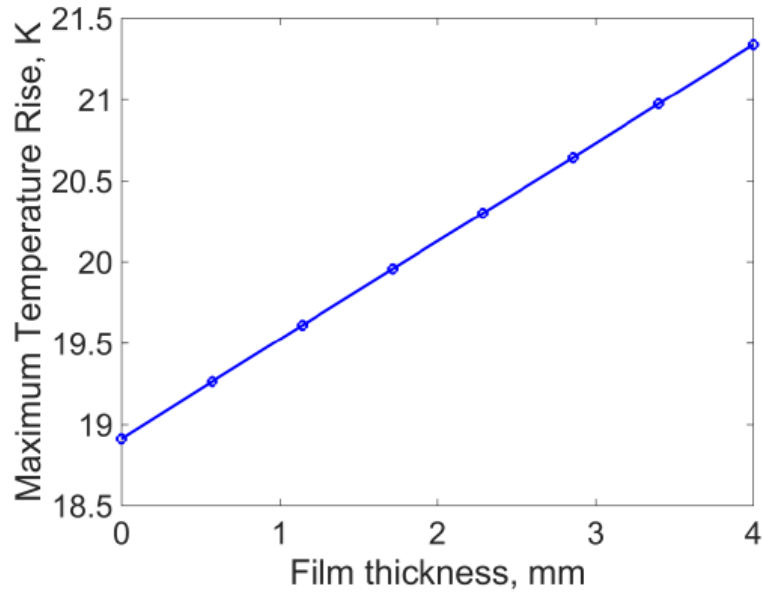


Figure 3.9: Peak Temperature Rise as a Function of Interface Material Thickness

Finally, Figure 3.9 analyzes the effect of a non-heat-generating plate inserted between the Li-ion cell and the coolant flow. This could be done in practice to physically separate the heat-generating cell from the coolant. However, doing so would result in increased temperature rise in the cell due to the additional thermal resistance of the plate. As discussed in Section 2, the iterative analytical model accounts for this by including an additional, one-dimensional thermal resistance during the process of interfacing the solid and fluid heat transfer models. Figure 3.9 plots the peak temperature in the cell operating at 5C as a function of the thickness of the interface plate, which is assumed to be made of a plastic material of thermal conductivity of 1.0 W/mK. Figure 3.9 shows a significant impact of the interface plate on the cell temperature, which worsens with increasing plate

thickness. This highlights an important consideration in pack-level thermal management design.

Design trade-offs such as those illustrated above are difficult to analyze using finite-element simulation tools due to computational complexity. On the other hand, such trade-offs can be easily analyzed using the iterative analytical method described here, which allows rapid analysis of the impact of various design choices as well as the effect of various geometric parameters and thermophysical properties on the performance of pack-level thermal management.

It should be noted that a significant shortcoming of the analytical model presented here is that it is limited to analysis of steady-state performance. Transient conditions are often relevant for the operation of Li-ion battery pack, in which case the model presented here must be expanded to account for transient phenomena. In general, deriving transient solutions is not straightforward, particularly for the flow problem in the fluid domain. Nevertheless, the present model provides useful guidelines for designing thermal management systems for Li-ion battery pack, as demonstrated in Figures 3.1 through 3.9.

CHAPTER 4

CONCLUSIONS

Heat removal from a Li-ion cell battery pack is critical not only for safety and reliability, but also for optimal performance. Analytical models such as the one presented in this work may be helpful in analyzing and optimizing the design of pack-level thermal management systems involving the removal of heat generated in cells with a coolant flow. Such models help determine the effect of various parameters on cooling efficiency, and help identify optimal parametric design spaces. Such analytical models are also important for multiphysics co-optimization, since several thermal management related parameters also profoundly affect the electrochemical performance of the cell. By developing a robust model for analyzing heat transfer in a fluid-cooled Li-ion battery pack, this research contributes towards improved thermal and electrochemical performance.

APPENDIX A
NOMENCLATURE

h	Convective heat transfer coefficient
H	Height
k	Thermal conductivity
L	Length
Pr	Prandtl number
q''	Heat flux
\dot{Q}'''	Volumetric heat generation rate
Re	Reynolds number
T	Temperature
u,v	Velocity components
α	Thermal diffusivity
0	Interface
f	Fluid
s	Solid
x,y	Coordinates

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BIOGRAPHICAL INFORMATION

Divya Chalise is an undergraduate pursuing an Honors Bachelor of Science in Mechanical Engineering. He has conducted research in the Microscale Thermophysics Lab with Dr. Ankur Jain for nearly three years and has authored and co-authored four journal papers. His research includes analytical modeling, finite element analysis and molecular dynamics study of heat transfer in Li-ion cells. In summer 2017, Divya was selected for the Summer Undergraduate Research Fellowship (SURF) program of Purdue University, where he worked in the Nanoscale Energy Transport and Conversion Lab with Dr. Xiulin Ruan. At Purdue, he contributed towards developing two computational tools based on molecular dynamics.

His research interest is in studying fundamental problems in energy transport and conversion. After graduation, Divya plans to attend graduate school to obtain a Ph.D. in Mechanical Engineering.